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FLUID MECHANICS

CIVIL ENGINEERING

Date of Test : 07/10/2024

ANSWER KEY >

1. (d)	7. (a)	13. (c)	19. (b)	25. (b)
2. (a)	8. (b)	14. (b)	20. (b)	26. (b)
3. (c)	9. (d)	15. (a)	21. (d)	27. (c)
4. (b)	10. (c)	16. (a)	22. (c)	28. (a)
5. (b)	11. (d)	17. (c)	23. (c)	29. (b)
6. (d)	12. (a)	18. (b)	24. (b)	30. (c)

DETAILED EXPLANATIONS

1. (d)

Kinetic energy correction factor is given by

$$\alpha = \frac{1}{AV^3} \int u^3 dA$$

2. (a)

Given, $\rho = 981 \text{ kg/m}^3$
 and $\tau = 0.2452 \text{ N/m}^2$

Velocity gradient, $\frac{du}{dy} = 0.2 \text{ s}^{-1}$

Now, using the equation

$$\tau = \mu \frac{du}{dy}$$

$$\Rightarrow 0.2452 = \mu \times 0.2$$

$$\Rightarrow \mu = \frac{0.2452}{0.2} = 1.226 \text{ Ns/m}^2$$

Kinematic viscosity is given by

$$\begin{aligned} \nu &= \frac{\mu}{\rho} = \frac{1.226}{981} = 0.125 \times 10^{-2} \text{ m}^2/\text{sec} \\ &= 12.5 \text{ cm}^2/\text{sec} \\ &= 12.5 \text{ stokes} \end{aligned}$$

3. (c)

Continuity equation must be satisfied

$$\therefore \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\Rightarrow \frac{\partial}{\partial x}(ax + by) + \frac{\partial}{\partial y}(dx + cy) = 0$$

$$\Rightarrow a + c = 0$$

4. (b)

5. (b)

For parallel pipes, head loss through the pipe is equal,

$$\begin{aligned} h_{f_1} &= h_{f_2} \\ \Rightarrow \frac{f_1 L_1 V_1^2}{2gd_1} &= \frac{f_2 L_2 V_2^2}{2gd_2} \end{aligned}$$

$$\Rightarrow \frac{500 \times (0.5)}{0.3 \times 800} \times 2 \times 9.81 \times 0.35 = V_2^2 \quad \left(\frac{V_1^2}{2g} = 0.5 \text{ m} \right)$$

$$\Rightarrow V_2 = 2.674 \text{ m/s}$$

Discharge through pipe 2,

$$Q = A_2 V_2$$

$$= \frac{\pi}{4} (0.35)^2 \times 2.476 = 0.2573 \text{ m}^3/\text{s}$$

6. (d)

7. (a)

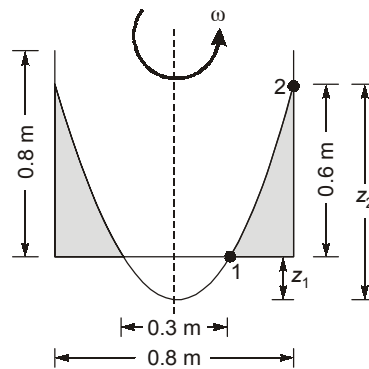
$$P_A - H \times 9.81 \times 1 - 0.18 \times 9.81 \times 0.827 = P_B - 13.6 \times 9.81 \times (H + 0.53)$$

$$- H \times 9.81 - 1.4603 = 97 - 13.6 \times 9.81 \times H - 13.6 \times 9.81 \times 0.53$$

$$\Rightarrow H = 0.2245 \text{ m}$$

$$\therefore H = 22.45 \text{ cm}$$

8. (b)



$$z_2 - z_1 = \frac{\omega^2}{2g} [R_2^2 - R_1^2]$$

$$0.6 = \frac{\omega^2}{2g} [0.4^2 - 0.15^2]$$

$$\omega = 9.253 \text{ rad/sec}$$

$$\frac{2\pi N}{60} = 9.253$$

$$N = 88.36 \text{ rpm}$$

9. (d)

In Navier's-Stoke equation viscous force term is considered and in all the above mentioned flow viscous force can't be neglected.

10. (c)

$$K = 2.1 \times 10^9 \text{ Pa}; E = 2.1 \times 10^{11} \text{ Pa}$$

$$\rho = 1000 \text{ kg/m}^3; D = 400 \text{ mm}$$

$$t = 4 \text{ mm}$$

Velocity of propagation of water hammer pressure

$$= \sqrt{\frac{K/\rho}{1 + \frac{KD}{Et}}} = \sqrt{\frac{2.1 \times \frac{10^9}{1000}}{1+1}} = 1024.7 \text{ m/s}$$

11. (d)

In steady uniform flow

Shear friction velocity, $V_* = \sqrt{\frac{\tau_0}{\rho}}$... (i)

Also, $V_* = \sqrt{\frac{f}{8}} \times V_{avg}$... (ii)

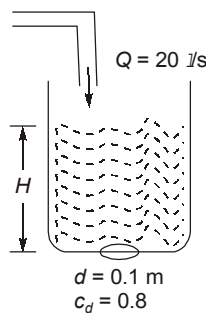
From eq. (i) and (ii)

$$\sqrt{\frac{\tau_0}{\rho}} = \sqrt{\frac{f}{8}} \times V_{avg}$$

Squaring both sides, $\frac{\tau_0}{\rho} = \frac{f}{8} \times V_{avg}^2$

$$\Rightarrow \tau_0 = \frac{0.024}{8} \times 2 \times 2 \times 1000 = 12 \text{ N/m}^2$$

12. (a)



Assume H is the level of water in the tank in steady condition.

For steady water level in the tank

Discharge through orifice

= Water enters in the tank

$$c_d a \sqrt{2gH} = 20 \times 10^{-3}$$

$$0.8 \times \frac{\pi}{4} (0.1)^2 \sqrt{2gH} = 0.02$$

$$H = 0.52 \text{ m}$$

13. (c)

Given: $u = xe^{-kt}$ and $v = y$

Equation of a streamline is given by

$$\frac{dx}{u} = \frac{dy}{v}$$

$$\Rightarrow \frac{dx}{xe^{-kt}} = \frac{dy}{y} \quad \left[\text{Let } e^{-kt} = \lambda \right]$$

$$\Rightarrow \frac{dx}{xk} = \frac{dy}{y}$$

$$\therefore \ln x = k \ln y + \ln d$$

where 'd' is a constant.

$$\Rightarrow \ln x = \ln y^\lambda + \ln d$$

$$\Rightarrow x = dy^\lambda$$

$$\Rightarrow y^\lambda = \frac{1}{d}x$$

$$\Rightarrow y = \left(\frac{1}{d}\right)^{1/\lambda} x^{1/\lambda} = Cx^{1/e^{-kt}} \quad \left[\text{where } \left(\frac{1}{d}\right)^{1/\lambda} = C \right]$$

$$\Rightarrow y = Cx^{e^{kt}}$$

14. (b)

Given data:

Relative density of glass sphere = 2.7

Diameter of glass sphere = 1 mm

Velocity of sphere = 1.25 cm/s

Density of oil = 920 kg/m³

$$\text{Reynold's number} = \frac{\rho v d}{\mu}$$

Let us assume that Stokes' law is valid then,

$$V = \frac{1}{18} D^2 \left(\frac{\gamma_s - \gamma_f}{\mu} \right)$$

$$\frac{1.25}{100} = \frac{1}{18} \times \frac{(10^{-3})^2 (2.7 \times 1000 \times 9.81 - 920 \times 9.81)}{\mu}$$

$$\mu = 0.0776 \text{ Pa.S}$$

$$\text{Reynold's number} = \frac{\rho V D}{\mu} = \frac{920 \times \frac{1.25}{100} \times 10^{-3}}{0.0776} = 0.148 < 1$$

Hence Stokes law is valid.

Therefore dynamic viscosity, $\mu = 0.0776 \text{ Pa.S}$

15. (a)

Distance from the centre where average velocity equal is to local velocity = $\frac{R}{\sqrt{2}}$

$$\therefore \text{Distance from boundary of pipe} = R - \frac{R}{\sqrt{2}} = 150 \left(1 - \frac{1}{\sqrt{2}} \right) \text{ mm} = 4.39 \text{ cm}$$

16. (a)

$$\begin{aligned} \text{Discharge ratio, } Q_r &= \frac{Q_m}{Q_p} = L_{rh} (L_{rv})^{3/2} \\ &= \frac{1}{625} \times \left(\frac{1}{36} \right)^{3/2} = \frac{1}{135000} \end{aligned}$$

$$\begin{aligned} \therefore Q_p &= \frac{Q_m}{Q_r} = 0.025 \times 135000 \\ &= 3375 \text{ m}^3/\text{s} \end{aligned}$$

17. (c)

Reynold number,

$$Re_x = \frac{u_\infty x}{\nu} = \frac{2 \times 1}{1.5 \times 10^{-5}} = 1.33 \times 10^5$$

$$\delta = \frac{4.64x}{\sqrt{Re_x}} = \frac{4.64 \times 1}{\sqrt{1.33 \times 10^5}} = 0.0127$$

$$\text{Now, } \frac{du}{dy} = u_\infty \left[\frac{3}{2} \cdot \frac{1}{\delta} - \frac{3}{2} \left(\frac{y^2}{\delta^3} \right) \right]$$

$$\left. \frac{du}{dy} \right|_{y=0} = \frac{3u_\infty}{2\delta}$$

Now, shear stress,

$$\tau_0 = \mu \left(\frac{du}{dy} \right)_{y=0} = \mu \times \frac{3u_\infty}{2\delta}$$

$$= \frac{3u_\infty \times \nu \times \rho}{2\delta}$$

$$\therefore \mu = \nu \rho$$

$$= \frac{3 \times 2 \times 1.5 \times 10^{-5} \times 1.23}{2 \times 0.0127}$$

$$= 4.36 \times 10^{-3} \text{ N/m}^2$$

18. (b)

Buoyancy force acts through center of gravity of displaced liquid.

A large metacentric height in a vessel improves stability and makes time period of oscillation shorter.

19. (b)

20. (b)

$$\bar{u} = \frac{R^2}{8\mu} \left(\frac{\Delta P}{L} \right)$$

$$\frac{32\mu\bar{u}}{D^2} = \frac{\Delta P}{L}$$

$$\Rightarrow \frac{128\mu Q}{\pi D^4} = \frac{\Delta P}{L} = 2535 \text{ Pa}$$

21. (d)

τ_1 = shear stress at bottom

$$= \mu_1 \times \frac{V}{x}$$

$$\tau_2 = \text{shear stress at top} = \mu_2 \frac{V}{a-x}$$

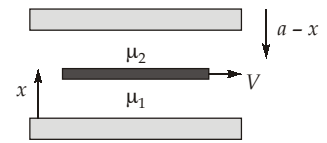
$$\text{drag force} = (\tau_1 + \tau_2) \times A = F_D$$

$$= F_D = A \times \left[\frac{\mu_1 V}{x} + \frac{\mu_2 V}{a-x} \right]$$

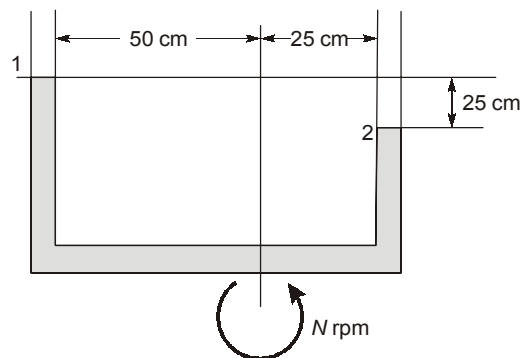
$$\frac{dF_D}{dx} = 0 = \frac{-\mu_1 V}{x^2} + \frac{\mu_2 V}{(a-x)^2} \Rightarrow \frac{\mu_1}{x^2} = \frac{\mu_2}{(a-x)^2}$$

$$a-x = \sqrt{\frac{\mu_2}{\mu_1}} x$$

$$\Rightarrow \frac{a\sqrt{\mu_1}}{\sqrt{\mu_1} + \sqrt{\mu_2}} = x$$



22. (c)



$$\frac{P_1}{\rho g} - \frac{V_1^2}{2g} + Z_1 = \frac{P_2}{\rho g} - \frac{V_2^2}{2g} + Z_2$$

$$Z_1 - Z_2 = \frac{V_1^2}{2g} - \frac{V_2^2}{2g}$$

$$0.25 = \frac{1}{2g} \{ r_1^2 \omega^2 - r_2^2 \omega^2 \}$$

$$0.25 \times 2 \times 9.81 = \omega^2 \left\{ \left(\frac{50}{100} \right)^2 - \left(\frac{25}{100} \right)^2 \right\}$$

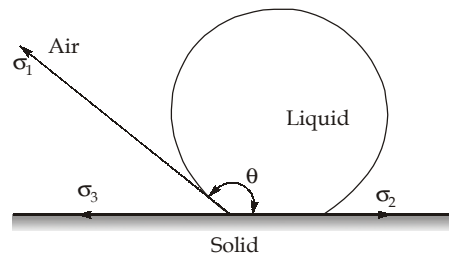
$$\omega = 5.115 \text{ rad/s}$$

$$N = \frac{60\omega}{2\pi} = \frac{60 \times 5.115}{2 \times \pi}$$

$$= 48.8 \text{ rpm}$$

23. (c)

From force balance at point of contact,



$$\sigma_1 \cos(180 - \theta) + \sigma_3 = \sigma_2$$

or $\cos(180 - \theta) = \frac{\sigma_2 - \sigma_3}{\sigma_1} = -\cos\theta$

\therefore

$$\sigma_1 = 0.0720 \text{ N/m (liquid and air)}$$

$$\sigma_2 = 0.0418 \text{ N/m (liquid and solid)}$$

$$\sigma_3 = 0.0008 \text{ N/m (air and solid)}$$

$$\cos\theta = \frac{0.0008 - 0.0418}{0.072} = -0.56944$$

$$\theta = 124.7^\circ$$

24. (b)

$$\text{Area of shaded region} = \frac{\pi \times 4^2}{4} - \frac{1}{2} \times \frac{8}{\sqrt{2}} \times \frac{4}{\sqrt{2}}$$

$$= 4\pi - 8 = 4.566 \text{ m}^2$$

Horizontal force, $F_H = \rho g A \bar{x}$

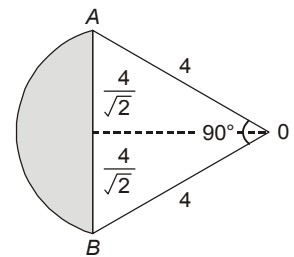
$$= 1000 \times 9.81 \times \frac{8}{\sqrt{2}} \times \frac{4}{\sqrt{2}}$$

$$F_H = 156.96 \times 10^3 \text{ N}$$

Vertical force, $F_V = 4.566 \times 9.81 \times 10^3$

$$= 44.79246 \times 10^3 \text{ N}$$

\therefore $\frac{F_H}{F_V} = \frac{156.96}{44.9246} = 3.504$



25. (b)

Hagen-Poiseuille's equation,

$$\Delta p = \frac{32\mu VL}{d^2}$$

where
$$V = \frac{Q}{A} = \frac{Q}{\frac{\pi}{4}d^2} = \frac{4Q}{\pi d^2}$$

$$\therefore \Delta p = \frac{128\pi QL}{\pi d^4}$$

$$\Delta p \propto \frac{1}{d^4}$$

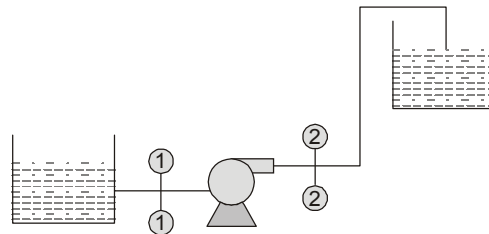
$$\Delta p \times d^4 = C$$

$$\Delta p_1 d_1^4 = \Delta p_2 d_2^4$$

$$\Delta p_1 \times d_1^4 = \Delta p_2 \times (2d_1)^4$$

or
$$\Delta p_2 = \frac{\Delta p_1}{16}$$

26. (b)



$$S = 0.8$$

$$\therefore \rho = 0.8 \times 1000 = 800 \text{ kg/m}^3$$

$$W_p = 50 \text{ J/kg}$$

$$V_1 = 1 \text{ m/s}$$

$$V_2 = 7 \text{ m/s}$$

Applying Bernoulli's equation between sections (1)-(1) and (2)-(2)

$$\frac{p_1}{\rho} + \frac{V_1^2}{2} + gz_1 + W_p = \frac{p_2}{\rho} + \frac{V_2^2}{2} + gz_2$$

where
$$z_1 = z_2$$

$$\frac{p_1}{\rho} + \frac{V_1^2}{2} + W_p = \frac{p_2}{\rho} + \frac{V_2^2}{2}$$

$$\frac{p_2 - p_1}{\rho} = \frac{V_1^2 - V_2^2}{2} + W_p$$

$$p_2 - p_1 = \rho \left[\frac{V_1^2 - V_2^2}{2} + W_p \right]$$

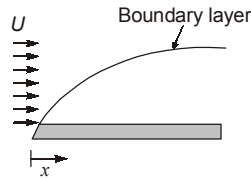
$$= 800 \left[\frac{(1)^2 - (7)^2}{2} + 50 \right] = 20800 \text{ N/m}^2 = 20.8 \text{ kN/m}^2$$

27. (c)

For laminar flow over flat plate,

$$\delta = \frac{5x}{\sqrt{Re}}$$

where $Re = \frac{Ux}{\nu}$



$$\therefore \delta = \frac{5x}{\left(\frac{Ux}{\nu}\right)^{1/2}}$$

$$\delta = \frac{5\sqrt{x}}{\sqrt{U/\nu}}$$

$$\delta \propto x^{1/2}$$

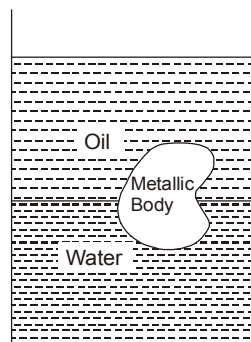
28. (a)

Let V = Volume of metallic body

45% of volume is in oil

i.e., $V_{oil} = 45\% \text{ of } V = 0.45V$

and $V_{water} = 0.55V$



For equilibrium condition,

$$\begin{aligned} \text{Net buoyant force} &= (F_B)_w + (F_B)_{oil} \\ &= \text{Weight of body} \end{aligned}$$

$$M_b g = \rho_w V_w g + \rho_{oil} V_{oil} g$$

$$M_b = \rho_w V_w + \rho_{oil} V_{oil}$$

$$\rho_b V = \rho_w \times 0.55V + \rho_{oil} \times 0.45V$$

or $\rho_b = \rho_w \times 0.55 + \rho_{oil} \times 0.45$

$$= 1000 \times 0.55 + 700 \times 0.45$$

$$= 550 + 315 = 865 \text{ kg/m}^3$$

29. (b)

For 2D-flow velocity field is:

$$\vec{V} = \frac{x}{x^2 + y^2} \hat{i} + \frac{y}{x^2 + y^2} \hat{j}$$

$$\text{so } u = \frac{x}{x^2 + y^2} \text{ and } v = \frac{y}{x^2 + y^2}$$

$$\begin{aligned} a_x &= u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \\ &= \frac{x}{x^2 + y^2} \frac{\partial}{\partial x} \left[\frac{x}{x^2 + y^2} \right] + \frac{y}{x^2 + y^2} \frac{\partial}{\partial y} \left[\frac{x}{x^2 + y^2} \right] \\ &= \frac{x}{x^2 + y^2} \left[\frac{x(-2x)}{(x^2 + y^2)^2} + \frac{1}{x^2 + y^2} \right] + \frac{y}{x^2 + y^2} \left[\frac{-x(2y)}{(x^2 + y^2)^2} \right] \\ &= \frac{-2x^3}{(x^2 + y^2)^3} + \frac{x}{(x^2 + y^2)^2} - \frac{2xy^2}{(x^2 + y^2)^3} \\ &= \frac{-2x^3 + x(x^2 + y^2) - 2xy^2}{(x^2 + y^2)^3} \\ &= \frac{-2x^3 + x^3 + xy^2 - 2xy^2}{(x^2 + y^2)^3} = \frac{-x^3 - xy^2}{(x^2 + y^2)^3} \\ &= \frac{-x(x^2 + y^2)}{(x^2 + y^2)^3} \end{aligned}$$

$$a_x = \frac{x}{(x^2 + y^2)^2}$$

$$\begin{aligned} a_y &= u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \\ &= \frac{x}{x^2 + y^2} \frac{\partial}{\partial x} \left[\frac{y}{x^2 + y^2} \right] + \frac{y}{x^2 + y^2} \frac{\partial}{\partial y} \left[\frac{y}{x^2 + y^2} \right] \\ &= \frac{x}{x^2 + y^2} \frac{(-2xy)}{(x^2 + y^2)^2} + \frac{y}{x^2 + y^2} \times \left[\frac{-2y^2}{(x^2 + y^2)^2} + \frac{1}{x^2 + y^2} \right] \\ &= \frac{-2x^2y}{(x^2 + y^2)^3} - \frac{2y^3}{(x^2 + y^2)^3} + \frac{y}{(x^2 + y^2)^2} \\ &= \frac{-2x^2y - 2y^3 + y(x^2 + y^2)}{(x^2 + y^2)^3} = \frac{-x^2y - y^3}{(x^2 + y^2)^3} = \frac{-y(x^2 + y^2)}{(x^2 + y^2)^3} \\ a_y &= \frac{-y}{(x^2 + y^2)^2} \end{aligned}$$

30. (c)

Given velocity field,

$$\vec{V} = (-x^2 + 3y)\hat{i} + (2xy)\hat{j}$$

where $u = -x^2 + 3y$ and $v = 2xy$

The acceleration components along x and y -axis.

$$a_x = u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y}$$

and
$$a_y = u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y}$$

$$= (-x^2 + 3y) \times (-2x) + 2xy \times 3$$

$$= 2x^3 - 6xy + 6xy = 2x^3$$

and
$$a_y = (-x^2 + 3y) \times 2y + 2xy \times 2x$$

$$= -2yx^2 + 6y^2 + 4x^2y = 2yx^2 + 6y^2$$

At point (1, -1),

$$a_x = 2$$

and
$$a_y = 2 \times (-1) \times 1 + 6 \times (-1)^2$$

$$= -2 + 6 = 4$$

$$\vec{a} = a_x\hat{i} + a_y\hat{j} = 2\hat{i} + 4\hat{j}$$

Resultant acceleration,

$$a = \sqrt{4 + 16} = \sqrt{20}$$

$$= \sqrt{4 \times 5} = 2\sqrt{5}$$

