

# POSTAL

## Book Package

# 2023

## Mechanical Engineering

### Conventional Practice Sets

#### Heat Transfer

#### *Contents*

<b>Sl. Topic</b>	<b>Page No.</b>
1. Introduction and Basic Concepts .....	2 - 6
2. Steady State Heat Conduction .....	7 - 25
3. Steady State Heat Conduction with Heat Generation .....	26 - 35
4. Heat Transfer from External Surfaces (Fins) .....	36 - 51
5. Transient Conduction .....	52 - 57
6. Forced Convection .....	58 - 76
7. Natural Convection .....	77 - 83
8. Heat Exchangers .....	84 - 99
9. Radiation Heat Transfer .....	100 - 118
10. Condensation and Boiling .....	119 - 123



**MADE EASY**  
Publications

**Note:** This book contains copyright subject matter to MADE EASY Publications, New Delhi. No part of this book may be reproduced, stored in a retrieval system or transmitted in any form or by any means. Violators are liable to be legally prosecuted.

## 5

## CHAPTER

## Transient Conduction

## Practice Questions : Level-I

- Q1** A steel ball of diameter 60 mm is initially in thermal equilibrium at 1030°C in a furnace. It is suddenly removed from the furnace and cooled in ambient air at 30°C, with convective heat transfer coefficient  $h = 20 \text{ W/m}^2\text{K}$ . The thermo-physical properties of steel are : density  $\rho = 7800 \text{ kg/m}^3$ , conductivity  $k = 40 \text{ W/mK}$  and specific heat  $c = 600 \text{ J/kgK}$ . The time required in seconds to cool the steel ball in air from 1030°C to 430°C is

**Solution:**

Diameter of ball,  $d = 60 \text{ mm} = 0.06 \text{ m}$ ;

Ambient temperature,  $T_0 = 30^\circ\text{C}$ ;

Density,  $\rho = 7800 \text{ kg/m}^3$ ;

Specific heat,  $c = 600 \text{ J/kgK}$ ;

Time,  $t = ?$

Initial temperature,  $T_i = 1030^\circ\text{C}$

Convective heat transfer coefficient,  $h = 20 \text{ W/m}^2\text{K}$

Conductivity,  $k = 40 \text{ W/mK}$

Final temperature of steel ball,  $T = 430^\circ\text{C}$

The temperature distribution relation is given by

$$\frac{T - T_0}{T_i - T_0} = e^{-\frac{ht}{\rho cl}} \quad \left[ \text{where } l = \frac{V}{A} \text{ characteristic length of balls} \right] \quad \dots(i)$$

$$\therefore V = \frac{\pi}{6} d^3, A = \pi d^2$$

$$\therefore l = \frac{V}{A} = \frac{\pi}{6} \frac{d^3}{\pi d^2} = \frac{d}{6} = \frac{0.06}{6} = 0.01 \text{ m}$$

Substituting the values of  $T$ ,  $T_0$ ,  $T_i$ ,  $h$ ,  $\rho$ ,  $c$  and  $l$  in Eq. (i), we get

$$\frac{430 - 30}{1030 - 30} = e^{\frac{-20 \times t}{7800 \times 600 \times 0.01}}$$

$$0.4 = e^{-4.273 \times 10^{-4} t}$$

Taking  $\log_e$  both sides, we get

$$\log_e 0.4 = -4.273 \times 10^{-4} \times t \times 1$$

or

$$t = \frac{0.9162}{4.273 \times 10^{-4}} = 2144.16 \text{ s}$$

- Q2** Stainless steel ball bearings having diameter of 1.2 cm are to be quenched in water. The balls leave the oven at 900°C and are exposed to air at 30°C for a while before they are dropped in water. If the temperature of the balls is not to fall below 850°C prior to quenching and the heat transfer coefficient in the air is 125 W/m²K, determine how long they can stand in the air before being dropped into the water. Following properties of stainless steel may be used:

$\rho = 8085 \text{ kg/m}^3$ ,  $k = 15.1 \text{ W/mK}$ ,

$c_p = 0.480 \text{ kJ/kgK}$ ,  $\alpha = 3.91 \times 10^{-6} \text{ m}^2/\text{s}$

**Solution:**

Given data:  $T_i = 900^\circ\text{C}$ ;  $T_\infty = 30^\circ\text{C}$ ;  $h = 125 \text{ W/m}^2\text{K}$ ;  $T = 850^\circ\text{C}$ ; Time taken =  $t = ?$

Since Metallic steel balls are of small size,

$$\text{Bi} = \frac{hl}{K} = \frac{hR}{3K} = \frac{125 \times 0.6 \times 10^{-2}}{3 \times 15.1} = 0.016$$

$\frac{hl}{k} = \text{Biot No} < 0.1 \Rightarrow \text{Lumped heat analysis is valid}$

$$\therefore e^{\left(\frac{hA}{\rho V c_p}\right)t} = \frac{T_i - T_\infty}{T - T_\infty}$$

Put

$$\frac{A}{V} = \frac{3}{R}$$

$$\Rightarrow 125 \times \frac{3}{\left(\frac{0.6}{100}\right)} \times \frac{1}{8085} \times \frac{1}{0.480 \times 10^3} \times t = \ln\left(\frac{900 - 30}{850 - 30}\right)$$

$\Rightarrow$  Time:  $t = 3.675 \text{ s}$

- Q3** A 4 mm thick panel of aluminium alloy ( $\rho = 2800 \text{ kg/m}^3$ ,  $c = 880 \text{ J/kgK}$  and  $k = 177 \text{ W/mK}$ ) is finished on both sides with an epoxy coating that must be cured at or above  $150^\circ\text{C}$  for atleast 5 min. The curing operation is performed in a large oven with air at  $175^\circ\text{C}$  and convection coefficient of  $h = 40 \text{ W/m}^2\text{K}$ . If the panel is placed in the oven at an initial temperature of  $30^\circ\text{C}$ , at what total elapsed time, will the cure process be completed?

**Solution:**

Given data:  $T_\infty = 175^\circ\text{C}$ ;  $h = 40 \text{ W/m}^2\text{K}$ ;  $\rho = 2800 \text{ kg/m}^3$ ,  $c = 880 \text{ J/kgK}$   
 $k = 177 \text{ W/mK}$

**Assumptions:**

1. Uniform heating
2. Constant properties

Characteristic length of plate,  $L_c = L = 2 \text{ mm}$

$$\text{Biot number, } Bi = \frac{hL_c}{k} = \frac{40 \times 2 \times 10^{-3}}{177} = 4.5198 \times 10^{-4}$$

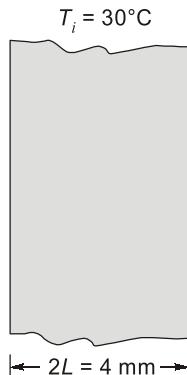
Since,  $Bi < 0.1$ , the lumped heat capacitance approximation can be used.

As we know,

$$\begin{aligned} \frac{T - T_\infty}{T_i - T_\infty} &= \exp\left[-\frac{hA}{\rho V c} t\right] = \exp\left[-\frac{h}{\rho L_c c} t\right] \\ \Rightarrow \frac{150 - 175}{30 - 175} &= \exp\left[-\frac{40}{2800 \times 0.002 \times 880} t\right] \\ t &= 216.57 \text{ s} \end{aligned}$$

Total time to complete the 5 min duration cure,

$$\begin{aligned} t_e &= t_i + t = (5 \times 60 + 216.57) \text{ s} \\ t_e &= 516.57 \text{ s} = 8.61 \text{ min} \end{aligned}$$



- Q4** A bearing piece in the form of half of a hollow cylinder of 60 mm ID, 90 mm OD and 100 mm long is to be cooled to  $-100^\circ\text{C}$  using a cryogenic gas at  $-150^\circ\text{C}$  with a convective heat transfer coefficient of 70  $\text{W/m}^2\text{K}$ . Determine the time required. Take properties of bearing material as  $c = 444 \text{ J/kgK}$ ,  $\rho = 8900 \text{ kg/m}^3$  and  $k = 17.2 \text{ W/mK}$ .

**Solution:**

Given: A piece of bearing as half of hollow cylinder with

$$D_1 = 60 \text{ mm} \quad \text{or} \quad r_1 = 0.03 \text{ m}$$

$$L = 100 \text{ mm} = 0.1 \text{ m},$$

$$T = 100^\circ\text{C}$$

$$k = 17.2 \text{ W/mK},$$

$$D_2 = 90 \text{ mm} \quad \text{or} \quad r_2 = 0.045 \text{ m}$$

$$T_i = 30^\circ\text{C}$$

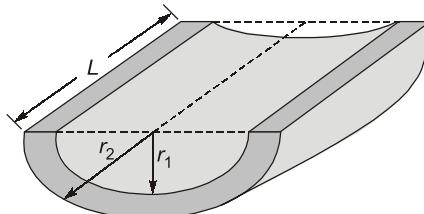
$$c = 444 \text{ J/kgK},$$

$$h = 70 \text{ W/m}^2\text{K}$$

$$T_\infty = -150^\circ\text{C}$$

$$\rho = 8900 \text{ kg/m}^3$$

To find: Time required to reach  $-100^\circ\text{C}$ .



The characteristic length of the cylinder.

The volume of bearing piece,

$$V = \left(\frac{1}{2}\right) \times \pi(r_2^2 - r_1^2)L = \left(\frac{1}{2}\right) \times \pi\{(0.045)^2 - (0.03)^2\} \times 0.1 \\ = 1.766 \times 10^{-4} \text{ m}^3$$

$$\text{Surface area of the bearing, } A_s = (\text{Front + back + lateral + longitudinal}) \text{ area} \\ = 2 \times (1/2)\pi(r_2^2 - r_1^2) + \pi L(r_1 + r_2) + 2 \times L \times (r_2 - r_1) \\ = \pi \times (0.045^2 - 0.03^2) + \pi \times 0.1 \times (0.03 + 0.045) \\ + 2 \times 0.1 \times (0.045 - 0.03) \\ = 3.53 \times 10^{-3} + 0.0235 + 3 \times 10^{-3} = 0.03003 \text{ m}^2$$

$$L_c = \frac{V}{A_s} = \frac{1.766 \times 10^{-4}}{0.03003} = 5.872 \times 10^{-3} \text{ m}$$

$$\text{Biot number, } B_i = \frac{hL_c}{k} = \frac{70 \times 5.872 \times 10^{-3}}{17.2} = 0.0239$$

Which is less than 0.1, hence the lumped heat capacity system analysis may be applied. Using for temperature distribution

$$\frac{T - T_\infty}{T_i - T_\infty} = \exp\left[-\frac{ht}{\rho L_c C}\right]$$

$$\text{Substituting the values, } \frac{-100 - (-150)}{30 - (-150)} = \exp\left\{-\frac{70t}{8900 \times 5.872 \times 10^{-3} \times 444}\right\}$$

$$\text{or, } t = 424.6 \text{ s}$$

### Practice Questions : Level-II

**Q5** A 15 mm diameter mild steel sphere ( $k = 42 \text{ W/m}^\circ\text{C}$ ) is exposed to cooling air flow at  $20^\circ\text{C}$  resulting in the convective coefficient  $h = 120 \text{ W/m}^2\text{C}$ . Determine the following:

- (i) Time required to cool the sphere from  $550^\circ\text{C}$  to  $90^\circ\text{C}$ .
- (ii) Instantaneous heat transfer rate 2 minutes after the start of cooling.
- (iii) Total energy transferred from the sphere during the first 2 minutes.

For mild steel take:  $\rho = 7850 \text{ kg/m}^3$ ,  $c = 475 \text{ J/kg}^\circ\text{C}$  and  $\alpha = 0.045 \text{ m}^2/\text{h}$ .

**Solution:**

Note: As unit of ' $\alpha$ ' is in 'hr' so time ' $t$ ' is taken in hours.

$$\text{Given: } R = \frac{15}{2} = 7.5 \text{ mm} = 0.0075 \text{ m}; \quad k = 42 \text{ W/m°C}; \quad T_{\infty} = 20^\circ\text{C}$$

$$T_i = 550^\circ\text{C}; \quad T = 90^\circ\text{C}; \quad h = 120 \text{ W/m}^2\text{°C}$$

**(i) Time required to cool the sphere from  $550^\circ\text{C}$  to  $90^\circ\text{C}$ ,  $t$ :**

The characteristics length  $L_c$  is given by,

$$L_c = \frac{\frac{4}{3}R^3}{4\pi R^2} = \frac{R}{3} = \frac{0.0075}{3} = 0.0025 \text{ m}$$

$$\text{Biot number, } B_i = \frac{hL_c}{k} = \frac{120 \times 0.0025}{42} = 0.007143$$

$$\text{Fourier number, } F_o = \frac{\alpha t}{L_c^2} = \frac{0.045 \times t}{(0.0025)^2} = 7200t \quad (\text{where } t \text{ is in hour})$$

Since  $B_i < 0.1$ , so we can use lump theory to solve this problem.

The temperature variation with time is given by

$$\boxed{\frac{T - T_{\infty}}{T_i - T_{\infty}} = e^{-B_i F_o}}$$

Substituting the values, we get

$$\frac{90 - 20}{550 - 20} = e^{-0.007143 \times 7200t} = e^{-51.43t}$$

$$0.132 = e^{-51.43t} \quad \text{or} \quad e^{51.43t} = \frac{1}{0.132} = 7.576$$

or,

$$51.4t = 2.025$$

or,

$$t = \frac{2.025}{51.43} = 0.03937h = 141.7 \text{ s}$$

**(ii) Instantaneous heat transfer rate 2 minutes (0.0333h) after the start of cooling,  $Q_1$ :**

$$\boxed{Q_i = -hA_s(T_i - T_{\infty})e^{-B_i F_o}}$$

Now,

$$B_i F_o = (0.007143)(7200 \times 0.0333) = 1.7126$$

∴

$$Q_i = 120 \times 4\pi \times (0.0075)^2 (550 - 20) e^{-1.7126} = -8.1 \text{ W}$$

The negative sign shows that heat is given off by sphere.

**(iii) Total energy transferred from the sphere during first 2 minutes (0.0333h)  $Q'$ :**

Amount of heat transfer during time interval,

$$(o, t) = \int_0^t \theta \cdot dt$$

$$= \int_0^t hA(T - T_{\infty}) \cdot dt = \int_0^{0.0333} hA(T_i - T_{\infty})e^{-B_i F_o} \cdot dt$$

$$\Delta V = \rho V c (T_i - T_{\infty}) [e^{-B_i F_o} - 1]$$

$$= 7850 \times \frac{4}{3} \pi \times (0.0075)^3 (475)(550 - 20) [e^{-1.7126} - 1]$$

$$= -2862.3 \text{ J}$$