

POSTAL Book Package

2023

Mechanical Engineering

Objective Practice Sets

Heat Transfer

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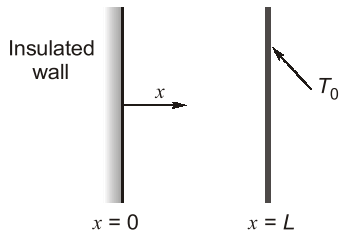
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Steady State Conduction with Heat Generation

MCQ and NAT Questions

- Q.1** Heat conduction equation in spherical coordinate system will be when temperature varies in r -direction only.
- (a) $\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \left(\frac{\partial T}{\partial r} \right) + \frac{q}{K} = \frac{1}{\alpha} \cdot \frac{\partial T}{\partial t}$
 (b) $\frac{\partial^2 T}{\partial r^2} + \frac{1}{2r} \frac{\partial T}{\partial r} + \left(\frac{q}{K} \right) = \frac{1}{2\alpha} \cdot \left(\frac{\partial T}{\partial t} \right)$
 (c) $\frac{\partial^2 T}{\partial r^2} + \frac{2}{r} \left(\frac{\partial T}{\partial r} \right) + \left(\frac{q}{K} \right) = \frac{1}{\alpha} \cdot \left(\frac{\partial T}{\partial t} \right)$
 (d) $\frac{\partial^2 T}{\partial r^2} + \frac{2}{r} \left(\frac{\partial T}{\partial r} \right) + \left(\frac{q}{2K} \right) = \frac{1}{\alpha} \cdot \left(\frac{\partial T}{\partial t} \right)$
- Q.2** The temperature drop in a plane wall with uniformly distributed heat generation can be decreased by reducing
- (a) wall thickness
 (b) heat generation rate
 (c) thermal conductivity of wall material
 (d) convection coefficient at the surface
- Q.3** The temperature profile for heat conduction through a wall of constant thermal conductivity in the presence of heat source is
- (a) a straight line (b) parabolic
 (c) logarithmic (d) hyperbolic
- Q.4** For a cylindrical rod with uniformly distributed heat sources, the thermal gradient dt/dr at half the radius location will be
- (a) one-fourth of that at the surface
 (b) one-half of that at the surface
 (c) twice of that at the surface
 (d) four times of that at the surface
- Q.5** A plane wall 10 cm thick generating heat at the rate of 4×10^4 W/m³ when an electric current is passed through it. The convective heat transfer coefficient between each face of wall and the ambient air is 50 W/m²-K. The ambient air temperature 20°C and $K = 15$ W/m-k. The maximum temperature in the wall is
- (a) 43.33°C (b) 53.33°C
 (c) 63.33°C (d) 73.33°C
- Q.6** A copper wire of 25 mm, carries 200 A and has a resistance of 0.4×10^{-4} ohms/cm length. The heat loss is
- (a) 100 W/m (b) 160 W/m
 (c) 1000 W/m (d) 1600 W/m
- Q.7** A 20 mm wire generates 3000 kW/m³ heat. If surface temperature is 200°C, the maximum temperature in the wire will be equal to (assume $K = 14$ W/m-k)
- (a) 205.4°C (b) 215.9°C
 (c) 219.2°C (d) 225.2°C
- Q.8** If ambient air temp is 10°C, the heat transfer coefficient between the wire surface and ambient air will be (in W/m²-k) in above problem.
- (a) 59 (b) 69
 (c) 79 (d) 89
- Q.9** For a long cylinder of radius R with uniformly distributed heat sources, the temperature distribution in the dimensionless form is
- (a) $\frac{t - t_w}{t_{\max} - t_w} = 1 - \frac{r}{R}$
 (b) $\frac{t - t_w}{t_{\max} - t_w} = 1 - \left(\frac{r}{R} \right)^2$
 (c) $\frac{t - t_w}{t_{\max} - t_w} = 1 - \left(\frac{r}{R} \right)^3$
 (d) $\frac{t - t_w}{t_{\max} - t_w} = 1 - \left(\frac{r}{R} \right)^4$
- where t_w is the temperature at the outer surfaces of the cylinder and t_{\max} is the temperature along the cylinder axis.
- Q.10** Heat transfer by conduction through hollow cylinder is given by
- (a) $Q = \frac{2\pi l(T_1 - T_2)}{k(r_2 - r_1)}$ (b) $Q = \frac{2\pi kl(T_1 - T_2)}{(r_2 - r_1)}$
 (c) $Q = \frac{2\pi kl(T_1 - T_2)}{\ln(r_2 / r_1)}$ (d) $Q = \frac{2\pi kl(T_1 - T_2)}{(r_1 + r_2)}$

Q.22 A slab of thickness L with one side ($x = 0$) insulated and other side ($x = L$) maintained at a constant temperature T_0 is shown below:



A uniformly distributed internal heat source produces heat in the slab at the rate of W/m^3 . Assume the heat conduction to be steady state and 1-D along the x -direction, the maximum temperature in the slab occurs at x equal to _____.

generation in a slab under steady state, 1-D heat conduction with uniform heat generation and constant thermal conductivity of material?

- (a) If one side of the slab is perfectly insulated, then maximum temperature will be at the another end of the slab (i.e. uninsulated side)
- (b) Temperature distribution is parabolic in nature in the slab.
- (c) Value of maximum temperature in the slab depends upon convection heat transfer coefficient of the liquid on the sides of the slab also.
- (d) If one side of the slab is an adiabatic wall, then maximum temperature will be at this side or at this surface.

Multiple Select Questions (MSQ)

- Q.23** A solid sphere of radius 0.5 m has an internal heat generation rate of $2 \times 10^6 W/m^3$. If the thermal conductivity of the material is $40 W/mK$ and the convective heat transfer coefficient at the surface of the sphere is $10 kW/m^2K$. Which of the following is/are correct, if the ambient temperature is $30^\circ C$?
- (a) The temperature at the outer surface is $63.33^\circ C$.
 - (b) The temperature at the outer surface is $163.32^\circ C$.
 - (c) The temperature at the centre is $2146.66^\circ C$.
 - (d) The temperature at the centre is $2246.66^\circ C$.

Q.24 Which of the following statements is/are correct with respect to conduction heat transfer with heat

- Q.25** Consider steady 1-D heat flow in a plate of 50 mm thickness with a uniform heat generation of $200 MW/m^3$. The left and right faces are kept at constant temperatures of $200^\circ C$ and $150^\circ C$ respectively. The plate has a constant thermal conductivity of $200 W/mK$. Which of the following statements is/are correct?
- (a) The location of maximum temperature within the plate from its left face is 26 mm.
 - (b) The location of maximum temperature within the plate from its left face is 24 mm.
 - (c) The maximum temperature within the plate is $488^\circ C$.
 - (d) The maximum temperature within the plate is $390^\circ C$.



Answers Steady State Conduction with Heat Generation

- | | | | | | | |
|---------|------------|---------------|------------|-------------|--------------|----------|
| 1. (c) | 2. (a) | 3. (b) | 4. (b) | 5. (c) | 6. (b) | 7. (a) |
| 8. (c) | 9. (b) | 10. (c) | 11. (c) | 12. (a) | 13. (a) | 14. (a) |
| 15. (d) | 16. (200) | 17. (0.0854) | 18. (700) | 19. (95.72) | 20. (365.34) | 21. (32) |
| 22. (0) | 23. (a, c) | 24. (b, c, d) | 25. (b, c) | | | |

Explanations Steady State Conduction with Heat Generation

1. (c)

Conduction equation in spherical form:

$$\frac{\partial^2 T}{\partial r^2} + \frac{2}{r} \left(\frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \psi} \frac{\partial}{\partial \psi} \left[\sin \psi \frac{\partial T}{\partial \psi} \right] + \frac{1}{r^2 \sin^2 \psi} \frac{\partial^2 T}{\partial \psi^2} + \frac{\dot{q}}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial \tau}$$

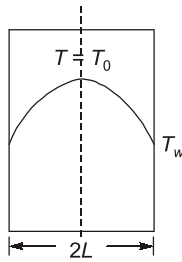
In one dimensional form it is

$$\frac{\partial^2 T}{\partial r^2} + \frac{2}{r} \left(\frac{\partial T}{\partial r} \right) + \frac{\dot{q}}{k} = \frac{1}{\alpha} \left(\frac{\partial T}{\partial \tau} \right)$$

2. (a)

Temperature drop in a plane with heat generation is

$$\Delta T = T_0 - T_w = \frac{\dot{q}L^2}{2K}$$



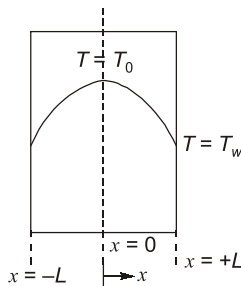
ΔT can be reduced by reducing wall thickness.

3. (b)

Temperature profile is,

$$T_0 - T = \frac{\dot{q} x^2}{k} \cdot \frac{1}{2}$$

\therefore Parabolic curve



4. (b)

The temperature distribution through a cylindrical rod with uniformly distributed heat sources is parabolic and prescribed as

$$t = t_w + \frac{q_g}{4K}(R^2 - r^2)$$

$$\frac{dt}{dr} = \frac{q_g}{4K}(-2r)$$

$$\left(\frac{dt}{dr}\right)_{r=R} = \frac{q_g}{4K} \times (-2 \times R)$$

$$\left(\frac{dt}{dr}\right)_{r=R/2} = \frac{q_g}{4K} \times \left(-2 \times \frac{R}{2}\right)$$

Apparently, $\left(\frac{dt}{dr}\right)_{r=R/2} = \frac{1}{2} \left(\frac{dt}{dr}\right)_{r=R}$

5. (c)

$$\begin{aligned} T_{\max} &= T_{\infty} + \frac{qL}{2h} + \frac{qL^2}{8K} \\ &= \left(60 + \frac{4 \times 10^4 \times (0.1)}{2 \times 50} + \frac{4 \times 10^4 \times (0.1)^2}{8 \times 15} \right) \\ &= 63.33^\circ\text{C} \end{aligned}$$

6. (b)

$$\begin{aligned} Q &= I^2 R = (200)^2 \times (0.4 \times 10^{-4}) \\ &= 1.6 \text{ W/cm} = 160 \text{ W/m} \end{aligned}$$

7. (a)

$$\begin{aligned} T_c &= T_o + \frac{q}{4K} \cdot r_o^2 \\ &= 200 + \frac{3000}{4 \times 14} \times (10 \times 10^{-3})^2 \times 10^3 \\ &= 205.4^\circ\text{C} \end{aligned}$$

8. (c)

$$\begin{aligned} \therefore T_o &= T_{\infty} + \frac{\dot{q} r_o}{2h} \\ \therefore h &= \frac{\dot{q} r_o}{2(T_o - T_{\infty})} \\ &= \frac{300 \times 10^3 \times 10 \times 10^{-3}}{2(200 - 10)} \\ &= 78.95 \approx 79 \text{ W/m}^2\text{k} \end{aligned}$$

9. (b)

The temperature distribution inside a cylinder with heat generation is a parabola i.e., a second degree equation. Hence, the correct answer is (b).

10. (c)

From Fourier law of heat conduction

$$Q = -kA \frac{dT}{dr}$$

For hollow cylinder

$$Q = -k(2\pi r l) \frac{dT}{dr}$$

$$\int_{r_1}^{r_2} Q \left(\frac{dr}{r} \right) = \int_{T_1}^{T_2} (-2\pi k l) dT$$

$$Q = \frac{2\pi k l}{\ln\left(\frac{r_2}{r_1}\right)} (T_1 - T_2)$$

11. (c)

