

2017

MADE EASY
WORKBOOK



**Detailed Explanations of
Try Yourself Questions**

**Mechanical Engineering
Refrigeration and Air-conditioning**



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— Publications

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Heat Engine, Heat Pump, Refrigerator and Reversed Carnot Cycle



Detailed Explanation of Try Yourself Questions

T1 : Solution

$$(\text{COP})_{\text{RE}} = (\text{COP})_{\text{HP}} - 1 = 4 - 1 = 3$$

$$(\text{COP})_{\text{RE}} = \frac{\text{Required cooling effect}}{\text{Power input}}$$

$$\begin{aligned} \Rightarrow \text{Required cooling effect} &= 3 \times 3 = 9 \text{ kW} \\ &= 9 \times 60 \text{ kJ/min} \\ &= 540 \text{ kJ/min} \end{aligned}$$

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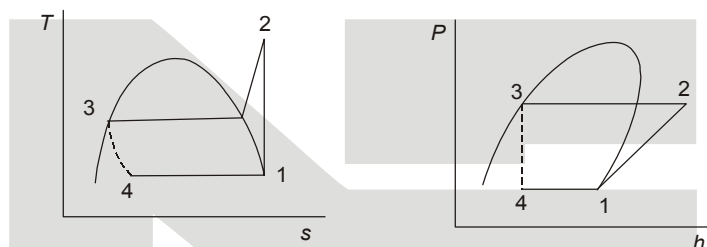
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Vapour Compression Refrigeration System



Detailed Explanation of Try Yourself Questions

T1 : Solution



From table

$$h_1 = 183.2 \text{ kJ/kg}$$

$$h_2 = 222.6 \text{ kJ/kg}$$

$$h_3 = h_4 = 84.9$$

[3 to 4 is an Isenthalpic process]

$$V_s = \frac{1.5}{1000} \text{ m}^3$$

$$N = 1600 \text{ m}^3$$

$$\eta_{\text{vol.}} = 80\% = \frac{80}{100} = 0.8$$

$$\eta_{\text{vol.}} = \frac{\dot{m}V_1}{V_s \times \frac{N}{60}}$$

∴

$$\frac{80}{100} = \frac{\dot{m} \times 0.0767}{\frac{1.5}{1000} \times \frac{1600}{60}}$$

$$\dot{m} = \frac{80}{100} \times \frac{1.5}{1000} \times \frac{1600}{60} \times \frac{1}{0.0767} = 0.4172 \text{ kg/s}$$

$$\begin{aligned} \text{R.E.} &= \dot{m}[h_1 - h_2] \\ &= 0.4172 \times [222.6 - 183.2] = 16.437 = 16.44 \text{ kW} \end{aligned}$$

T2 : Solution

$$h_4 = h_3 = 134 \text{ kJ/kg}$$

$$h_1 = 244 \text{ kJ/kg}$$

$$h_{2'} = 285 \text{ kJ/kg}$$

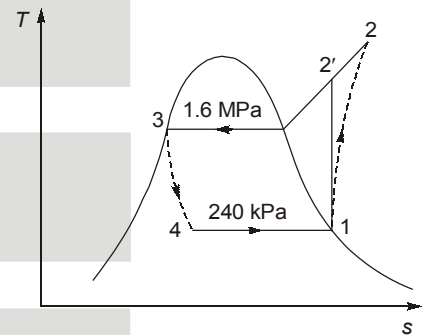
$$h_2 = h_1 + \frac{h_{2'} - h_1}{\eta_{\text{comp.}}}$$

$$= 244 + \frac{285 - 244}{0.85} = 292.2 \text{ kJ/kg}$$

$$\begin{aligned} Q_R &= (h_2 - h_3) = 292.2 - 134 \\ &= 158.2 \text{ kJ/kg} \end{aligned}$$

$$\begin{aligned} W_{\text{input}} &= h_2 - h_1 = 292.2 - 244 \\ &= 48.2 \text{ kJ/kg} \end{aligned}$$

$$\text{COP} = \frac{Q_R}{W_{\text{input}}} = \frac{158.2}{48.2} = 3.2821$$



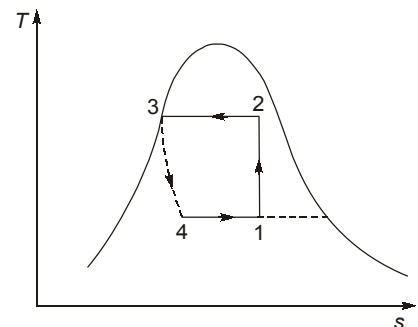
T3 : Solution

$$s_1 = s_{f1} + \frac{x_1 h_{fg1}}{T_1}$$

$$= 0.5443 + \frac{x_1 \times 1297.68}{263}$$

$$= 0.5443 + 4.934x_1$$

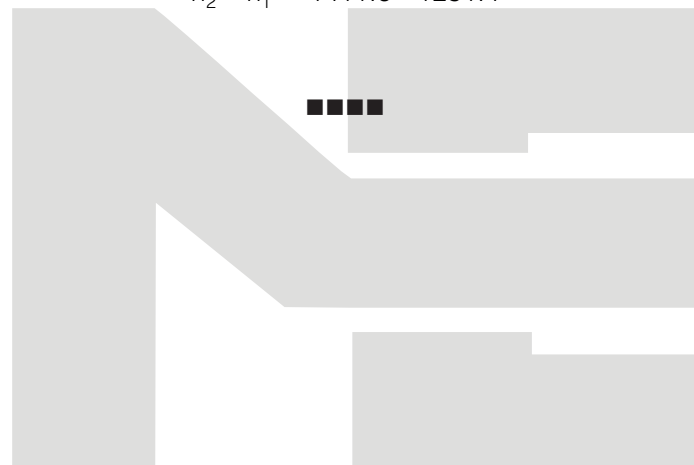
$$s_2 = s_{f2} + \frac{x_2 h_{fg2}}{T_2}$$



$$\begin{aligned}
 &= 1.2037 + \frac{0.95 \times 1145.8}{303} \\
 &= 4.796 \\
 0.5443 + 4.934 x_1 &= 4.796 \\
 x_1 &= 0.86 \\
 h_1 &= h_{f_1} + x_1 h_{fg_1} \\
 &= 135.37 + 0.86 \times 1297.68 \\
 &= 1251.4 \text{ kJ/kg} \\
 h_2 &= h_{f_2} + x_2 h_{fg_2} \\
 &= 323.08 + 0.95 \times 1145.8 \\
 &= 1411.6 \text{ kJ/kg}
 \end{aligned}$$

We know that theoretical C.O.P.

$$\begin{aligned}
 &= \frac{h_1 - h_{f_3}}{h_2 - h_1} = \frac{1251.4 - 323.08}{1411.6 - 1251.4} = 5.8
 \end{aligned}$$



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Vapour Absorption Refrigeration System



Detailed Explanation of Try Yourself Questions

T1 : Solution

$$\text{COP} = \frac{T_G - T_0}{T_G} \times \frac{T_R}{T_0 - T_R}$$

T_R = Evapourator Temperature

T_G = Generator Temperature

T_0 = Ambient Temperature (condenser temperature)

$$\begin{aligned} \text{COP} &= \frac{360 - 310}{360} \times \frac{260}{310 - 260} \\ &= 0.72 \end{aligned}$$

$$0.72 = \frac{T_G - 310}{T_G} \times \frac{250}{310 - 250}$$

$$T_G = 374.9 \text{ K}$$

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Refrigerants



Detailed Explanation *of* Try Yourself Questions

T1 : Solution

R-502 is an azeotrope. An azeotrope is a mixture of two or more refrigerants in which the liquid and vapour have the same composition at equilibrium. An azeotrope behaves like pure component refrigerants because there is no change in boiling temperature or shift in composition during phase change, equipment operation or leakage.

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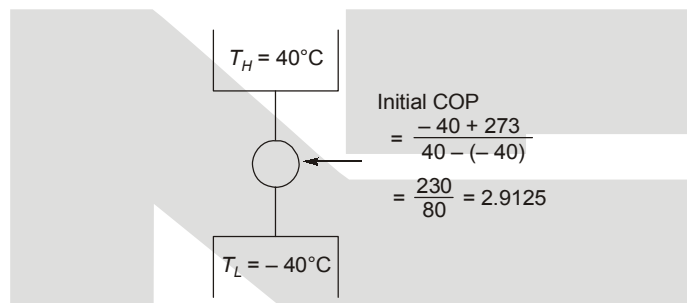
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Refrigeration Equipment and Gas Refrigeration



Detailed Explanation of Try Yourself Questions

T1 : Solution



Final COP = 3.5

Let the change in higher temperature and lower change be " ΔT ".

New higher temperature = $T_h - \Delta T$

New lower temperature = $T_L + \Delta T$,

$$[\text{COP}]_{\text{final}} = \frac{T_L + \Delta T}{(T_H - \Delta T) - (T_L + \Delta T)}$$

$$3.5 = \frac{233 + \Delta T}{(40 - \Delta T) - (-40 + \Delta T)}$$

$$3.5 = \frac{233 + \Delta T}{80 - 2\Delta T}$$

$$280 - 7\Delta T = 233 + \Delta T$$

$$280 - 233 = 7\Delta T + \Delta T$$

$$\Delta T = \frac{47}{8} = 5.875^\circ\text{C}$$

$$\begin{aligned}\text{Hence new higher temperature} &= 40 - 5.875 = 34.125^\circ\text{C} \\ &= 307.125 \text{ K}\end{aligned}$$

$$\begin{aligned}\text{New lower temperature} &= -40 + 5.875 \\ &= -34.125^\circ\text{C} \\ &= 238.875^\circ\text{C}\end{aligned}$$

Checking

$$\begin{aligned}\text{New COP} &= \frac{(T_L)_{\text{NEW}}}{(T_H)_{\text{NEW}} - (T_L)_{\text{NEW}}} \\ &= \frac{238.875}{307.125 - 238.875} = 3.5\end{aligned}$$



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Air-conditioning



Detailed Explanation of Try Yourself Questions

T1 : Solution

$P_{atm} = 1 \text{ bar} = 100 \text{ kPa}$
 $\text{DBT} = 30^\circ\text{C}$
 $\phi = 70\% = 0.7$
 $P_{vs} = 4.25 \text{ kPa}$

Specific humidity, $\omega = ?$

$$\phi = \frac{P_v}{P_{v_s}}$$

$$0.07 = \frac{P_v}{4.25}$$

$$P_v = 2.975 \text{ kPa}$$

Specific humidity,

$$\omega = 0.622 \times \frac{P_v}{P - P_v} = 0.622 \times \frac{2.975}{100 - 2.975}$$

$$= 0.0191 \frac{\text{kg water vapour}}{\text{kg dry air}}$$

T2 : Solution

Wet bulb depression at the inlet = $(t_{db} - t_{wb})_{\text{inlet}} = (38 - 18)_{\text{inlet}} = 20^\circ\text{C}$

Wet bulb depression at the outlet = $(24 - 18) = 6^\circ\text{C}$

Percentage change = $\frac{20 - 6}{20} = 70\%$

$(\because t_{wb \text{ inlet}} = t_{wb \text{ exit}})$

T3 : Solution

Inlet bulb depression at inlet

$$= DBT_1 - WBT_1$$

$$\text{Range} = T_{w1} - T_{w2}$$

$$\text{Approach} = T_{w2} - WBT_1$$

$$\text{Sum of range and approach} = T_{w1} - T_{w2} + T_{w2} - WBT_1$$

It is said wet bulb depression at inlet is equal to sum of approach and range

$$\therefore DBT_1 - WBT_1 = T_{w1} - T_{w2} + T_{w2} - WBT_1$$

$$DBT_1 = T_{w1}$$

$$\therefore DBT_1 - T_{w1} = 0$$

